

# Homogenisation techniques dedicated to paper industry: theory and applications.

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*Paris, 30 septembre 2010*

Part I –

Homogeneization theory applied  
to paper

Part II –

REV and X-Ray microtomography

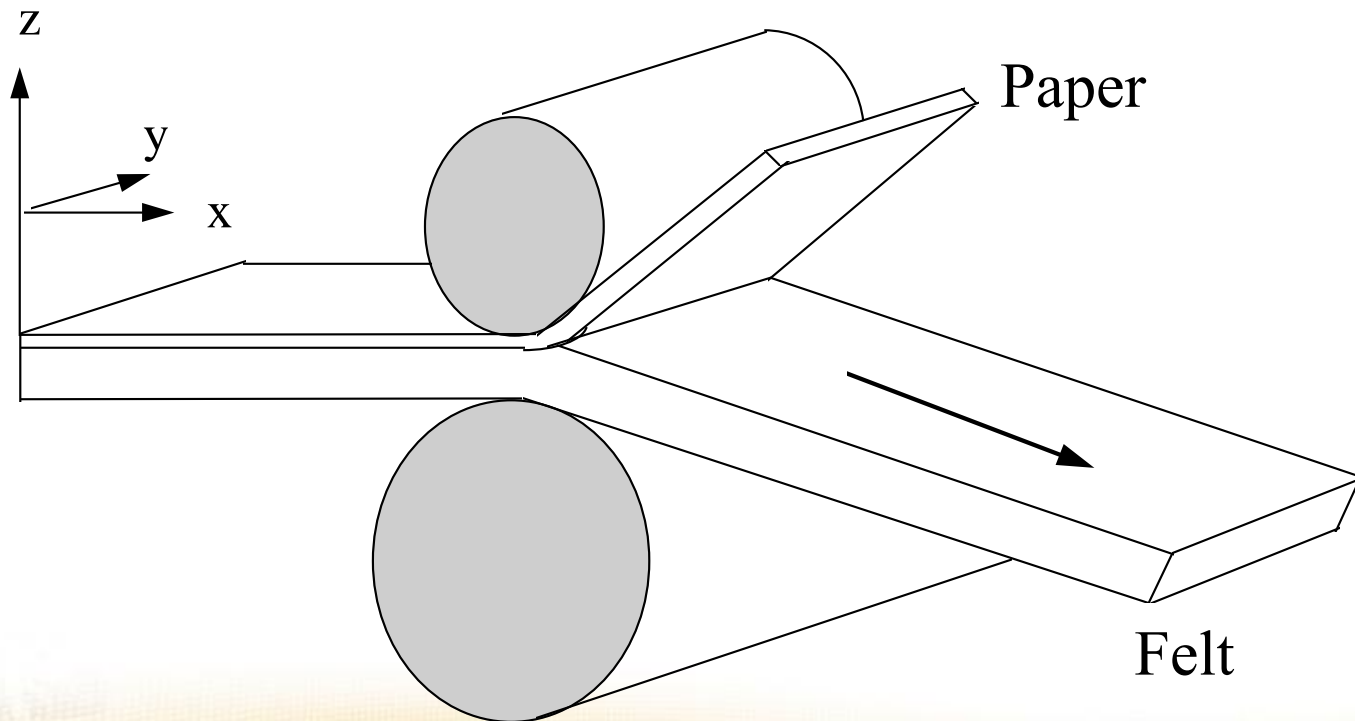
# Part I - CONTENT

- I - Introduction
- II - Method presentation
- III - Main Results
- IV - Example
- V - Conclusion

# I - INTRODUCTION

AIM :

Temperature field in paper during hot pressing



# I - INTRODUCTION (2)

Paper and Felt: deformable porous media

Non saturated: (non /) wetting phases

Complex structure at the pore scale

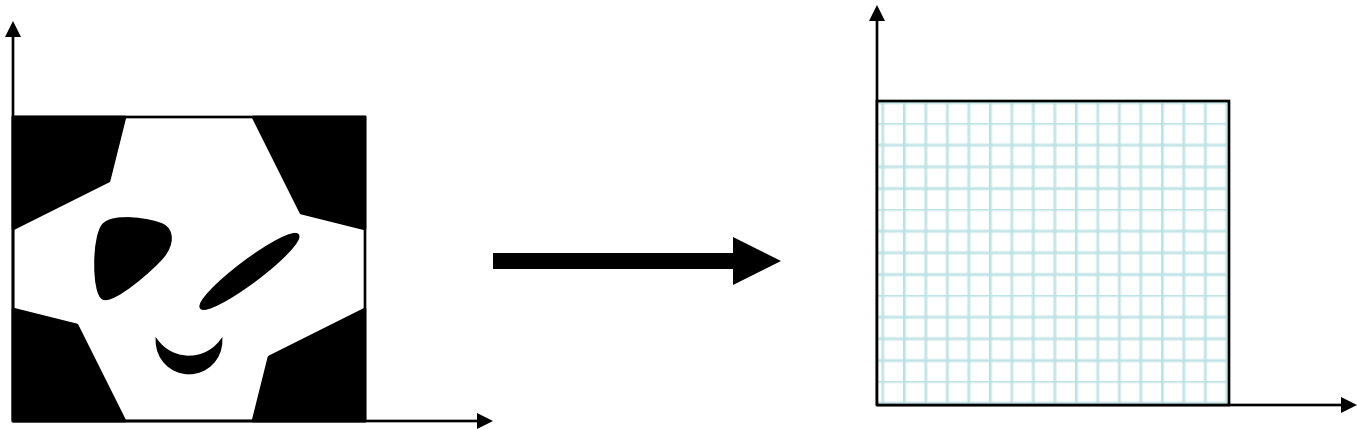
⇒ Macroscopic modelling:

Homogeneization

# I - INTRODUCTION (3)

Homogeneization:

microscale to macroscale



## EQUIVALENT POROUS MEDIUM



## II – METHOD PRESENTATION

The medium is assumed as periodic.

Random media yield similar  
macroscopic description modelling.

AURIAULT J.-L. (1991) "Heterogeneous medium. Is an equivalent macroscopic description possible?", Int. J. Engng. Sci., 29, 7, pages 785-795.



# II – METHOD PRESENTATION:

## Multiscale expansion method

- without macroscopic prerequisites,
- the macroscopic law,
- the effective parameters,
- the validity domain of the model.



## II – METHOD PRESENTATION:

Multiscale expansion method

### **SCALE SEPARATION**

pore dimension / sample size

$\Leftrightarrow$  model quality.



# II – METHOD PRESENTATION: Main steps

- 1 – Physical phenomena at the microscopic scale.
- 2 – Two different scales are defined ( $\varepsilon$ ).
- 3 – Physical Equations at microscopic scale.
- 4 – The dimensionless parameters are expressed in function of  $\varepsilon$ .



# II – METHOD PRESENTATION: Main steps (2)

5 – Asymptotic expansions in power of  $\varepsilon$  are introduced.

6 – Problems at different orders are solved to determine the successive approximations of the variables.

7 – Physical quantities are evaluated from the dimensionless ones.



# II – METHOD PRESENTATION

- The scale ratio  $\varepsilon = l / L$
- For a paper web, the characteristic lengths  
 $l = 10 \mu\text{m}$  and  $L = 1 \text{ mm}$   
 $\Rightarrow \varepsilon = 10^{-2}$
- Dimensionless parameters are evaluated in term of  $\varepsilon$ .

# II – METHOD PRESENTATION

Energy balance for a domain ( $k = w, a, s$ ):

$$\frac{\partial \rho_k C_{p_k} T_k}{\partial t} + \mathbf{v}_k \cdot \nabla (\rho_k C_{p_k} T_k) = \nabla \cdot (\rho_k \nabla T_k)$$

Flux conservation of heat on the interface:

$$\lambda_{kij} \left( \frac{\partial T_k}{\partial X_j} \right) N_i = \lambda_{lij} \left( \frac{\partial T_l}{\partial X_j} \right) N_i$$

Temperatures are continuous on each interface  
(no resistance) :

$$T_k = T_l$$

Dimensionless variables:  $X = X^* \cdot X^R$

Dimensionless parameters:

$$N_{\lambda_{aw}} = \frac{\lambda_a^R}{\lambda_w^R}$$

$$N_{\lambda_{sw}} = \frac{\lambda_s^R}{\lambda_w^R}$$

$$P = \frac{\left| \rho C_p \frac{\partial T}{\partial t} \right|^R}{\left| \frac{\partial}{\partial X_i} \lambda_{ij} \frac{\partial T}{\partial X_j} \right|^R}$$

$$Pe = \frac{\left| \rho C_p V_i \frac{\partial T}{\partial X_i} \right|^R}{\left| \frac{\partial}{\partial X_i} \lambda_{ij} \frac{\partial T}{\partial X_j} \right|^R}$$

(R)

- in  $\Omega_k$  :

$$P \frac{\partial \rho_k C_k T_k}{\partial t} = \frac{\partial}{\partial y_i} \left( \lambda_{kij} \frac{\partial T_k}{\partial y_j} \right) - Pe V_{ki} \frac{\partial \rho_k C_k T_k}{\partial y_i}$$

- in  $\Gamma_{kl}$  :

$$N_{\lambda_{kl}} \lambda_{kij} \left( \frac{\partial T_k}{\partial y_j} \right) N_i = \lambda_{lij} \left( \frac{\partial T_l}{\partial y_j} \right) N_i \quad (*)$$



# II – METHOD PRESENTATION

## - Reference Values

$(J \cdot m^{-1} \cdot s^{-1} \cdot K^{-1})$

$\lambda_s$

0.33

$\lambda_w$

0.602

$\lambda_a$

0.026

$(J \cdot kg^{-1} \cdot K^{-1})$

$C_{ps}$

$1.33 \cdot 10^3$

$C_{pw}$

$4.18 \cdot 10^3$

$C_{pa}$

$10^3$

$(kg \cdot m^{-3})$

$\rho_s$

$1.5 \cdot 10^3$

$\rho_w$

$10^3$

$\rho_a$

1.23



# II – METHOD PRESENTATION

$$N_{\lambda_{aw}} = 0.043 = O \left( \epsilon \right) \quad N_{\lambda_{sw}} = 0.548 = O \left( \epsilon \right)$$

$$P_w = \frac{C_w l^2}{\lambda_w \tau} = O \left( \epsilon^{-1} P_a \right)$$

$$P_s = \frac{C_s l^2}{\lambda_s \tau} = O \left( \epsilon_w \right)$$

# II – METHOD PRESENTATION

Each physical quantity  $\phi$  is then looked as:

$$\phi = \phi^{(0)} + \varepsilon \cdot \phi^{(1)} + \varepsilon^2 \cdot \phi^{(2)} + \varepsilon^3 \cdot \phi^{(3)} + \dots$$

Homogenisation process

$\Rightarrow$  approximated macroscopic models.

Model accuracies =  $O(\varepsilon)$

$\Rightarrow$  The larger the scale separation is,  
the better is the result (approximation).

## A - Small Péclet number: diffusion - convection

$$\mathbf{A-1:} \quad \mathbf{Pe} \leq \mathbf{O}(\varepsilon^2) \quad \mathbf{P} = \mathbf{O}(\varepsilon^2)$$

$$\langle C \rangle_{w,s} \frac{\partial T}{\partial t} = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) + \mathbf{O}(\varepsilon^2)$$

With :

$$\lambda_{ij}^{\text{eff}} = \frac{1}{|\Omega|} \int_{\Omega_w + \Omega_s} \lambda_{ij} \left( I_{kj} + \frac{\partial \chi_{Ik}}{\partial y_j} \right) d\Omega$$

$$\langle C \rangle_{w,s} = \frac{1}{|\Omega|} \int_{\Omega_w} C_w d\Omega + \int_{\Omega_s} C_s d\Omega$$

# III – MAIN RESULTS (2)

$$\mathbf{A-2 : Pe} \leq \mathbf{O}(\varepsilon^2) \quad \mathbf{P} \leq \mathbf{O}(\varepsilon^3)$$

$$0 = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) + \mathbf{O}(\varepsilon^3)$$

$$\mathbf{A-3 : Pe} = \mathbf{O}(\varepsilon) \quad \mathbf{P} = \mathbf{O}(\varepsilon^2)$$

$$\langle C \rangle_{w,s} \frac{\partial T}{\partial t} = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle C v_i \rangle_{\Omega} \frac{\partial T}{\partial x_i} + \mathbf{O}(\varepsilon^3)$$

J.-F. BLOCH, J.-L. AURIAULT, (1998) ‘Heat Transfer in Nonsaturated Porous Media: Modelling by Homogenisation’, *TiPM*, 30: 301–321.

# III - MAIN RESULTS (3)

$$\mathbf{A-4 : Pe} = \mathbf{O}(\varepsilon) \quad \mathbf{P} \leq \mathbf{O}(\varepsilon^3)$$

$$0 = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle C V_i \rangle_{\Omega} \frac{\partial T}{\partial x_i} + \mathbf{O}(\varepsilon)$$

$$\mathbf{A-5 : Pe}_{a,w} = \mathbf{O}(\varepsilon) \quad \mathbf{Pe}_s = \mathbf{O}(\varepsilon^2) \quad \mathbf{P} = \mathbf{O}(\varepsilon^2)$$

$$\langle C \rangle_{w,s} \frac{\partial T}{\partial t} = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle C V_i \rangle_{\Omega_a + \Omega_w} \frac{\partial T}{\partial x_i} + \mathbf{O}(\varepsilon)$$

# III - MAIN RESULTS (4)

## B - Higher Péclet number : dispersion

**B - 3 :  $Pe = O(1)$   $P \leq O(\varepsilon^3)$**

$$0 = \varepsilon \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{***\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega} \frac{\partial T}{\partial x_i} + O(\varepsilon^2)$$

$$\lambda_{ij}^{***\text{eff}} = \frac{1}{|\Omega|} \int_{\Omega_{w,s}} \left[ \lambda_{ij} \left( I_{ij} + \frac{\partial \chi_{IIIj}}{\partial y_1} \right) - C \chi_{V_i^{(0)}} \chi_{IIIj} \right] d\Omega$$

**B - 2 :  $Pe = O(1)$   $P = O(\varepsilon^2)$**

$$\varepsilon \langle C \rangle_{w,s} \frac{\partial T}{\partial t} = \varepsilon \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{***\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega} \frac{\partial T}{\partial x_i} + O(\varepsilon^2)$$



## B - Higher Péclet number : dispersion

**B - 1 : Pe = O(1) P = O(ε)**

$$\langle C \rangle_{\Omega_w + \Omega_s} + \varepsilon \langle C \rangle_{\Omega_a} \frac{\partial T}{\partial t} + \varepsilon \langle C \chi_{\Pi i} \rangle_{\Omega_w + \Omega_s} \frac{\partial^2 T}{\partial t \partial x_i} =$$

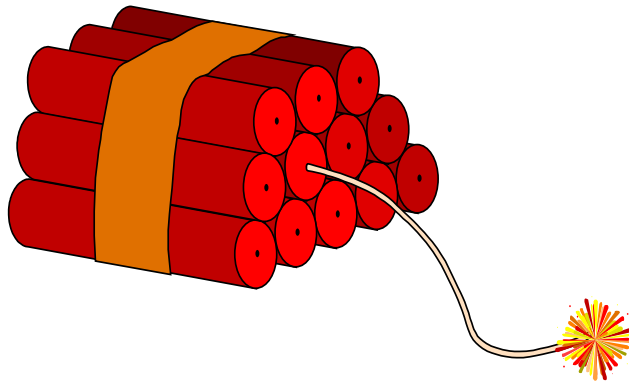
$$\varepsilon \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{**\text{eff}} \frac{\partial T}{\partial x_j} \right) - \left( \langle C V_i \rangle_{\Omega} \frac{\partial T}{\partial x_i} \right) + O(\varepsilon^2)$$

$$\lambda_{ij}^{**\text{eff}} = \frac{1}{|\Omega|} \int_{\Omega_{w,s}} \left[ \lambda_{ij} \left( I_{ij} + \frac{\partial \chi_{\Pi j}}{\partial y_1} \right) - C \langle V_i^{(0)} \chi_{\Pi j} \rangle \right] d\Omega$$



# III - MAIN RESULTS (6)

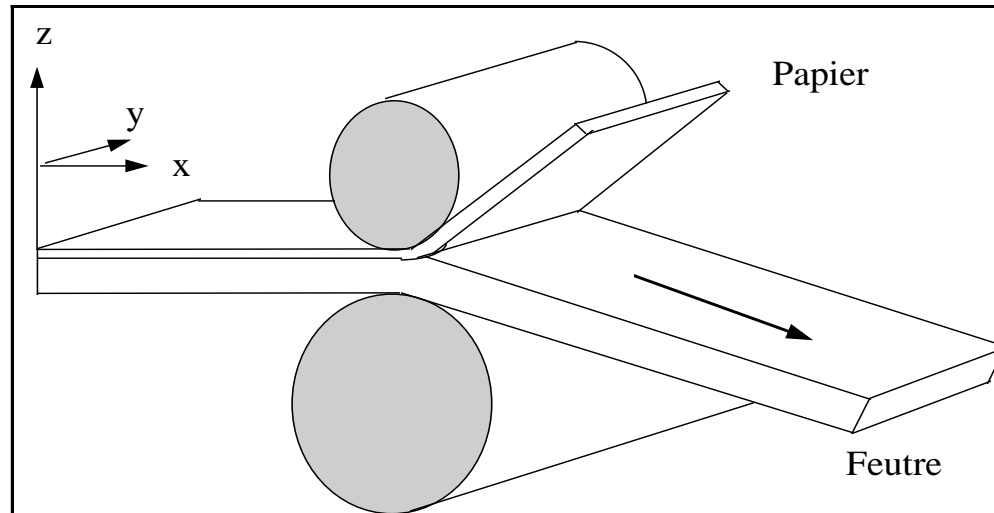
$$Pe \geq O(\varepsilon^{-1})$$



This case is NOT homogeneizable

$\Leftrightarrow$  no equivalent medium exists !

# IV - EXAMPLE: Hot pressing of a paper web



$$Pe = \frac{\rho \cdot C_p \cdot V \cdot l}{\lambda} \# \frac{10^3 \cdot 10^3 \cdot 10^{-2} \cdot 10^{-6}}{0.5} = 0 \left( 10^{-2} \right) \# 0 \left( 10^{-2} \right)$$



$$0 = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{eff} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega} \frac{\partial T}{\partial x_i}$$

# IV – EXAMPLE: Assumptions

$$0 = \frac{\partial}{\partial x_i} \left( \lambda_{ij}^{\text{eff}} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega} \frac{\partial T}{\partial x_i}$$

$$\lambda_w = 0 \quad \left( n_s \right)$$



$$0 = \frac{\partial}{\partial x_i} \left( \lambda_w \left( n_w + n_s \right) I_{ij} \frac{\partial T}{\partial x_j} \right) - \langle C V_i \rangle_{\Omega} \frac{\partial T}{\partial x_i}$$

$$n_s + n_w \neq 1.$$



$$0 = \frac{\partial}{\partial x_i} \left( \lambda_w I_{ij} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega} \frac{\partial T}{\partial x_i}$$

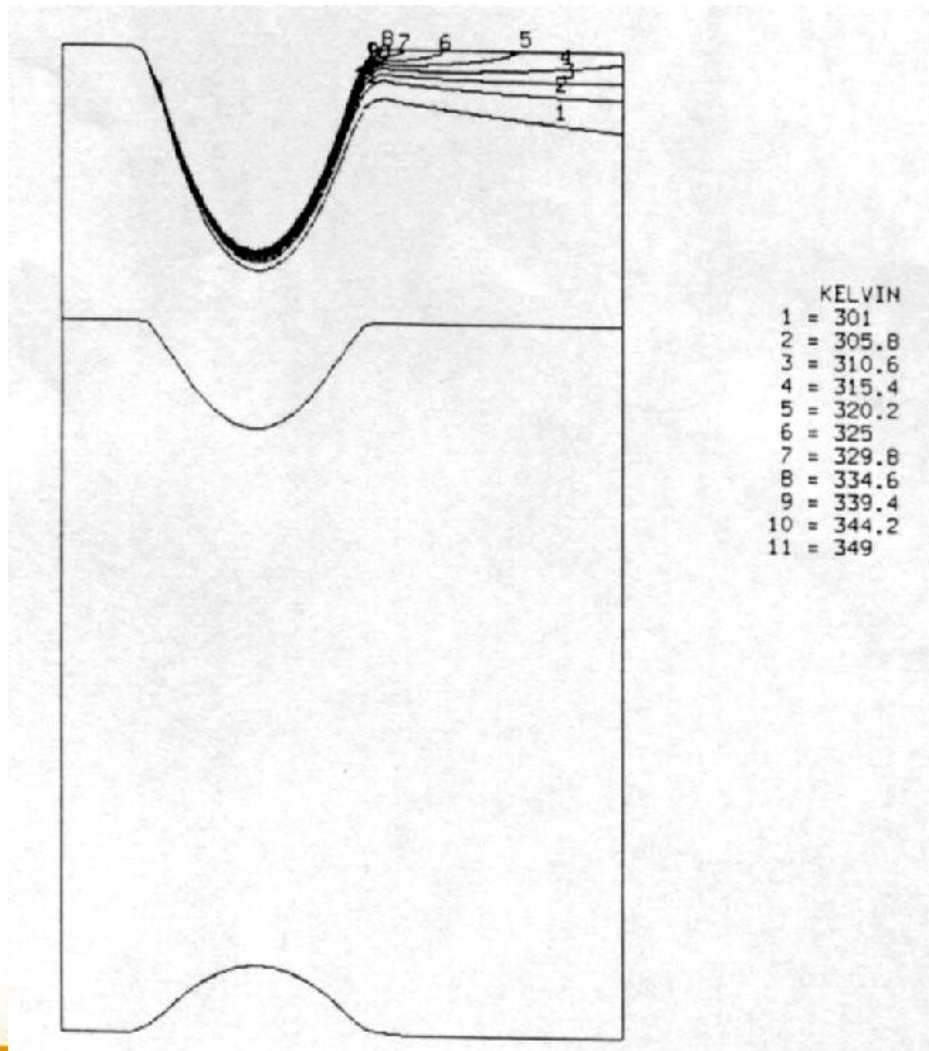
$$\rho_a C_{pa} V_a \ll \rho_w C_{pw} V_w$$



$$0 = \frac{\partial}{\partial x_i} \left( \lambda_w I_{ij} \frac{\partial T}{\partial x_j} \right) - \langle CV_i \rangle_{\Omega_s + \Omega_w} \frac{\partial T}{\partial x_i}$$

# IV - EXAMPLE:

## Temperature field in paper and felt



$$T_{\text{roll}} = 50 \text{ }^{\circ}\text{C}$$

Mach. Speed:  $10 \text{ m.s}^{-1}$ ,

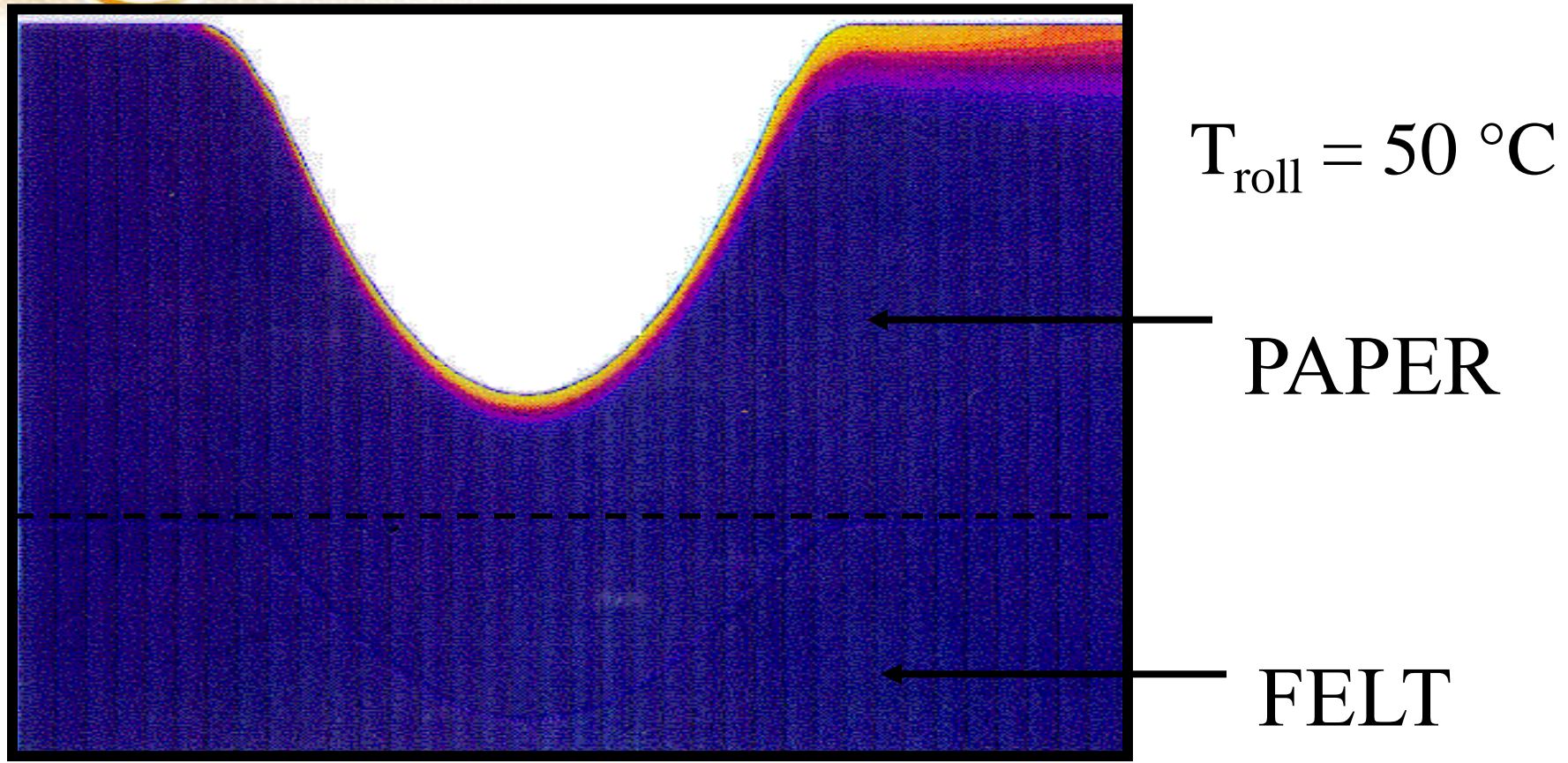
Paper thick.:  $320 \text{ } \mu\text{m}$ ,

Felt thick.:  $2.5 \text{ mm}$ ,

Nip Length:  $2.5 \text{ cm}$ .



# IV - EXAMPLE



Detail of temperature field in paper during hot pressing.

# V – CONCLUSIONS

## / Part I

- Same microscopic physics, different law structures, with different effective coefficients.
- Evaluating dimensionless numbers ( $\varepsilon$ ) :  
macroscopic model catalogue, their effective parameters and their validity domains are obtained.
- Physical characteristic values dedicated to the studied process.

# CONCLUSION / Part I (2)

- The equivalent description corresponds to a medium that reacts globally to the considered physical excitation like the microscopic medium studied.
- If the medium cannot be homogenised, macroscopic properties are not intrinsic to the media.
- Applicable to any porous medium that satisfies the microscopic hypotheses in use here.



## Part II

### 3D structure of Papers

/ VER

(X-Ray Microtomography)



# Estimation of paper physical properties based on synchrotron X-ray microtomography.

Jean-Francis Bloch

Sabine Rolland du Roscoat

Maxime Decain, Christian Geindreau

# Content (Partie Non présentée)

- I. Context
- II. Materials and Methods
- III. Estimation of paper structure / VER
  - Deterministic approach
  - Statistical approach
- I. Estimation of paper properties
- II. Conclusions and perspectives

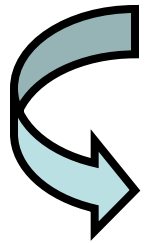


# I. Context

- Synchrotron X-ray microtomography gives access to the inner structure of samples at a micrometric scale
  - Quantification of the structure
  - Estimation of physical properties
- Comparison to experimental data

# I. Position of the problem

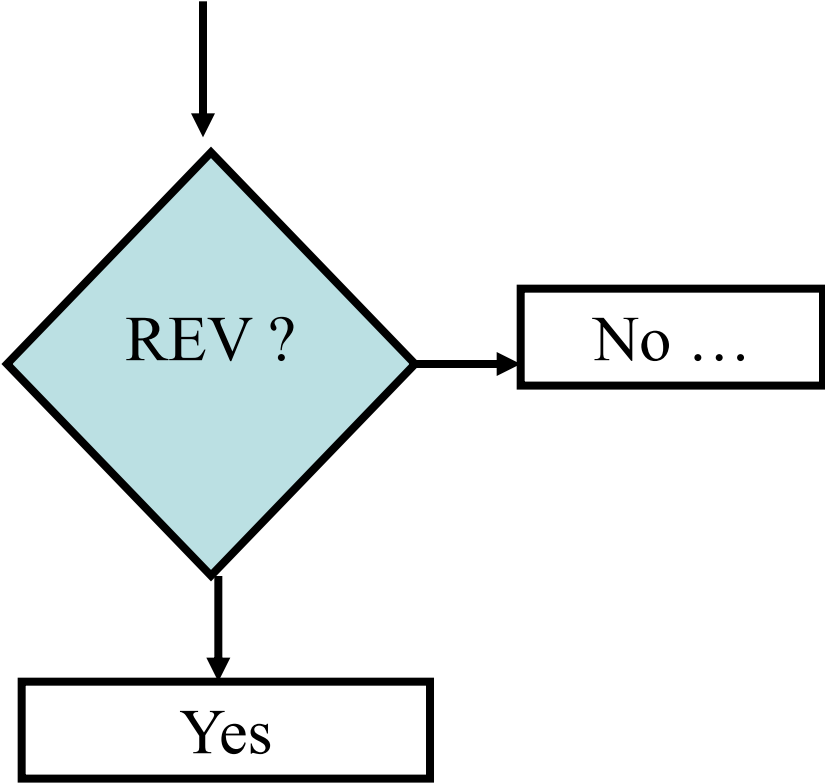
- May Physical properties be simulated from X-Ray microtomography?
- Analysed volume is much smaller than the characteristic lengths / physical properties?



Problem of the representativity for:

- Porosity and specific surface area
- Effective thermal conductivity and permeability

Tomographic data



Estimation of physical properties

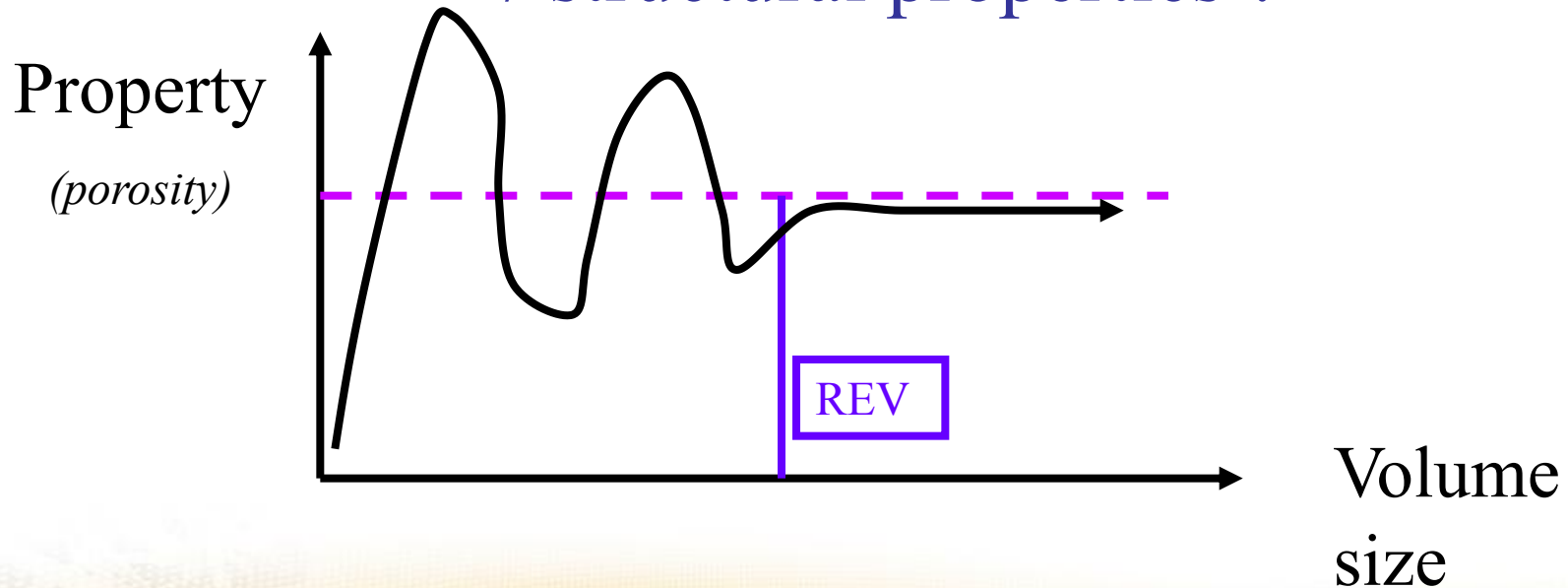
## II.4. Representative Elementary Volume

### REV

- Definition

Small samples (mm) !?

How Long is Long enough  
/ structural properties ?





## II.4. Applied methods

- Two approaches
  - Deterministic (classical)<sup>1</sup>
  - Statistical<sup>2</sup>

<sup>1</sup> W.J. Drugan, J.R. Willis, "A micromechanics-based nonlocal constitutive equation and estimates of representative volume element size for elastic composites.", J. Mech, Phys Solids, Vol. 44, No 4, 1996, pp 497-524.

<sup>2</sup> T. Kanit, S. Forest, I. Galliet, V. Mounoury, D. Jeulin, "Determination of the size of the representative volume element for random composites: statistical and numerical approach", International Journal of Solids and Structures 40, 2003, pp 3647-3679.

## III.5. Conclusions / Statistical REV

- Estimation of properties on volumes smaller than the deterministic REV



saving computing time in the case of the estimation of physical properties

Rolland du Roscoat, S., Decain, M., Thibault, X., Geindreau, C., Bloch J.-F. *Estimation of microstructural properties from synchrotron X-Ray microtomography and determination of the REV size in paper materials*. *Acta Materiala*, 55(8), 2007, 2841-2850

# Content

- I. Context
- II. Materials and Methods
- III. Estimation of paper structure / VER
  - Deterministic approach
  - Statistical approach
- IV. Estimation of paper properties
- V. Conclusions & perspectives

## IV.1. Estimation of permeability

- Estimation of tensor of permeability
  - No penetration of fluid into fibres
  - Pressure gradient is imposed at the interface
  - Estimation of the local fluid velocity
  - Deducing the permeability  
from Darcy Law

Koivu, V., Geindreau, C., Decain, M., Mattila, K., Bloch, J.-F., Kataja, M., *Transport properties of heterogeneous materials combining computerized x-ray micro-tomography and direct numerical simulations*, International Journal of Computational Fluid Dynamics, 23(10), 2010, 713-721