

# A New Look at the Modeling of Secondary Breakup

Nicolas Rimbert <sup>\*1,2</sup>, Sébastien Castrillon-Escobar<sup>1,2,3</sup>, Renaud Meignen<sup>3</sup>, Michel Gradeck<sup>1,2</sup>

<sup>1</sup>LEMMA, Université de Lorraine, Nancy France

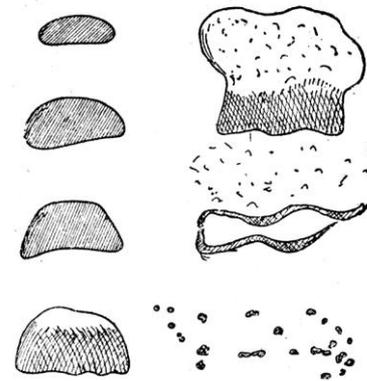
<sup>2</sup>CNRS, UMR 7563, Nancy, France

<sup>3</sup>IRSN, Service des accidents graves, Cadarache, France

\*Corresponding author: [nicolas.rimbert@univ-lorraine.fr](mailto:nicolas.rimbert@univ-lorraine.fr)

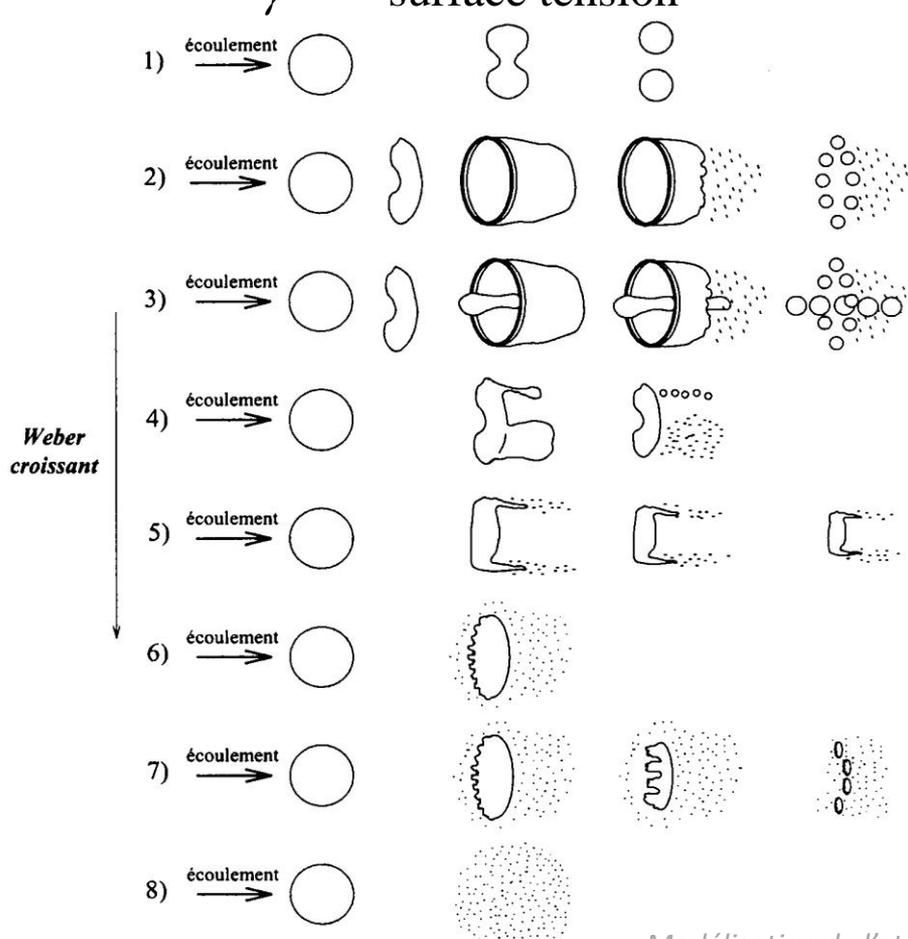
# Experimental studies

- Since Eotvos
  - **Drop tower**
    - Hochwelder (1919)
  - **Shock tube**
    - Ranger & Nicholls (1968)
    - Faeth's group in Michigan (90<sup>ies</sup>)
  - **Wind Tunnel**
    - Nowadays...
      - (Opfer et al. 2014, Kulkarni & Sojka 2014...etc.)
        - » Easier...
  - And many more...



# First Classification (Pilch and Erdman, 1987)

$$We = \frac{\rho U^2 L}{\gamma} = \frac{\text{inertia}}{\text{surface tension}}$$



1. *Deformation*  $We < 12$
2. *bag break-up*:  $12 < We < 50$
3. *umbrella break-up* for  $50 < We < 100$
4. *Multimode breakup*
5. *Shear break-up* for  $100 < We < 350$ )
6. *Wavy Shear Breakup*:  $350 < We$
7. *Piercing break-up*
8. *Catastrophic break-up*

# Second Classification (Faeth's Group)

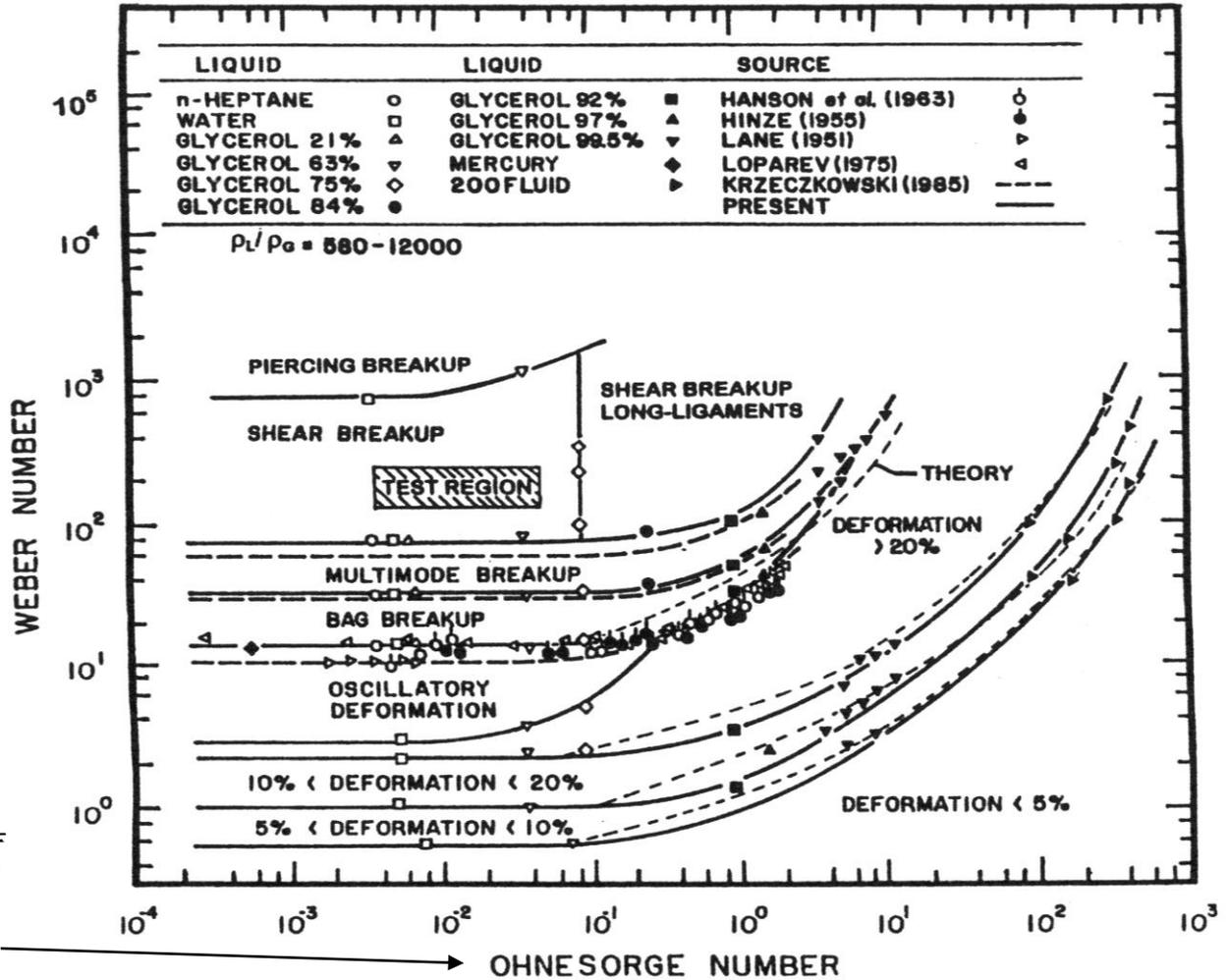
Regime map for shock wave disturbance  
 Univ. Ann Arbor

Hsiang and Faeth *Drop Deformation and breakup due to shock wave and steady disturbance*  
 IJMF, 21, 545-560, 1995

$$Oh = Z = \frac{\sqrt{We}}{Re} = \frac{\mu}{\sqrt{\gamma \rho D}}$$

Viscosity

$$= \frac{\text{Viscosity}}{\sqrt{\text{Inertia} \times \text{Surface Tension}}}$$

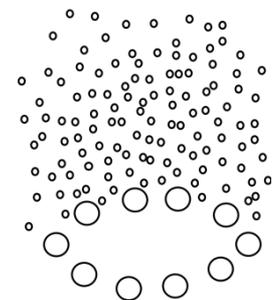
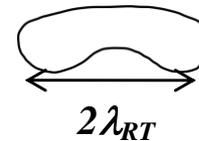
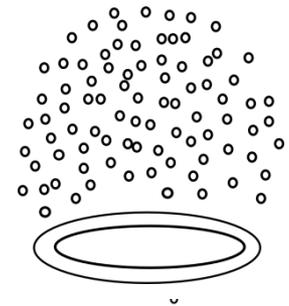
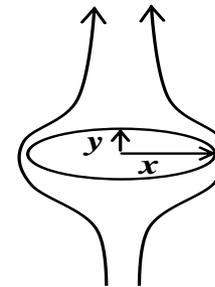
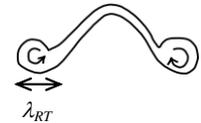
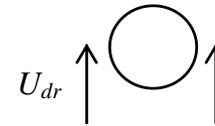


# Droplet Deformation Models

- Droplet deformation and breakup model
  - Oscillator-like Model
    - TAB Taylor Analogy Breakup (*O'Rourke 1987*)
    - DDB Droplet Deformation and Breakup (*Ibrahim et al. 1993*)
  - More recent
    - Elongational deformation (*Villermaux & Bossa 2009, Kulkarni & Sojka 2014*)
    - Potential flow around a disc (*Opfer et al. 2014*)
- A new model
  - Without fitting parameters... Is it possible?

# Bag-Breakup, Qualitatively

- In the literature
  - $12(23) < We < 50$
- Six stages
  - Inception
  - Deformation
  - RT Wave Growth
  - Bag Growth
  - Bag breakup
  - Rim Breakup



# Quantitatively

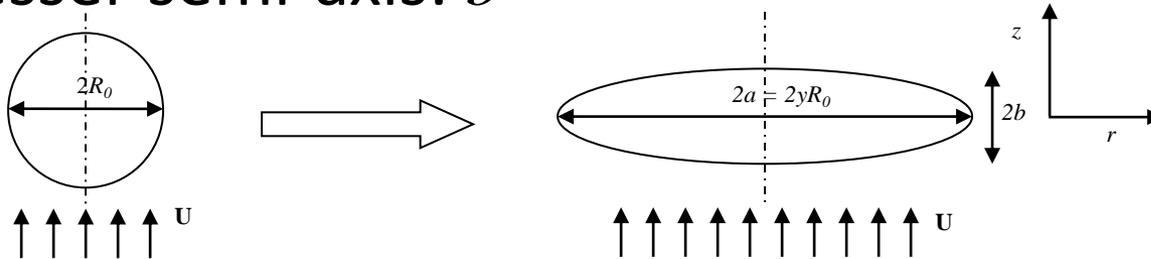
- Balance between:
  - Kinetic (deformation) energy:  $K$
  - Surface energy:  $E_s$
  - Viscous Dissipation:  $D$
  - Air Pressure Work:  $W_p$

$$\frac{dK}{dt} + \frac{dE_s}{dt} = W_p + D$$

- Simple modelling
  - Imposes a 1-parameter deformation path

# Hypotheses

- Chosen deformation path: Oblate Ellipsoid
  - Greater semi-axis:  $a$
  - Lesser semi-axis:  $b$



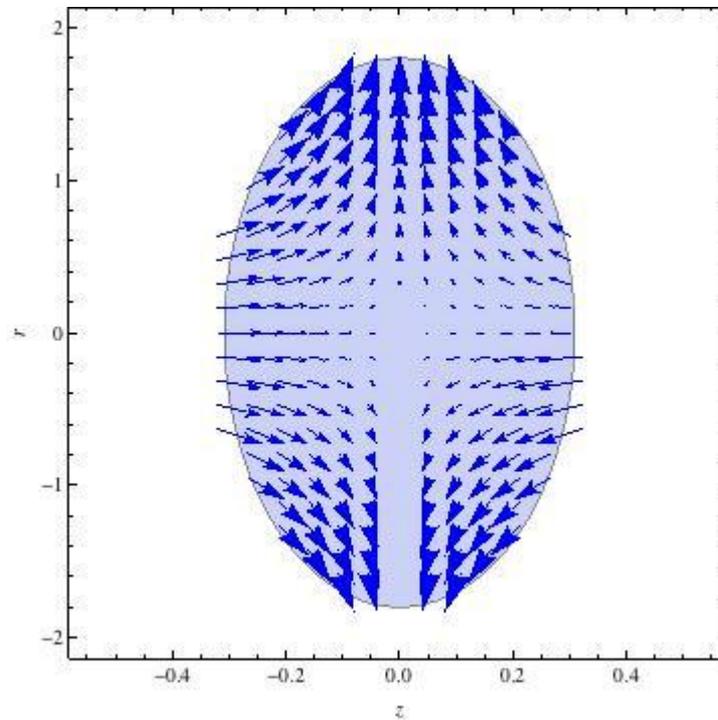
- Other hypotheses
  - Axisymmetric potential outside flow
  - Viscous extensional flow inside
  - Volume conservation  $a^2b = R_0^3$

# Flow inside the spheroid

- Viscous Extensional Flow

$$\begin{cases} v_r = \frac{\dot{\gamma}}{y} r \\ v_z = -2 \frac{\dot{\gamma}}{y} z \end{cases}$$

$$y = \frac{a}{R_0}$$



# Flow outside the spheroid

- Axisymmetric potential flow
  - Batchelor *An introduction to fluid dynamics*

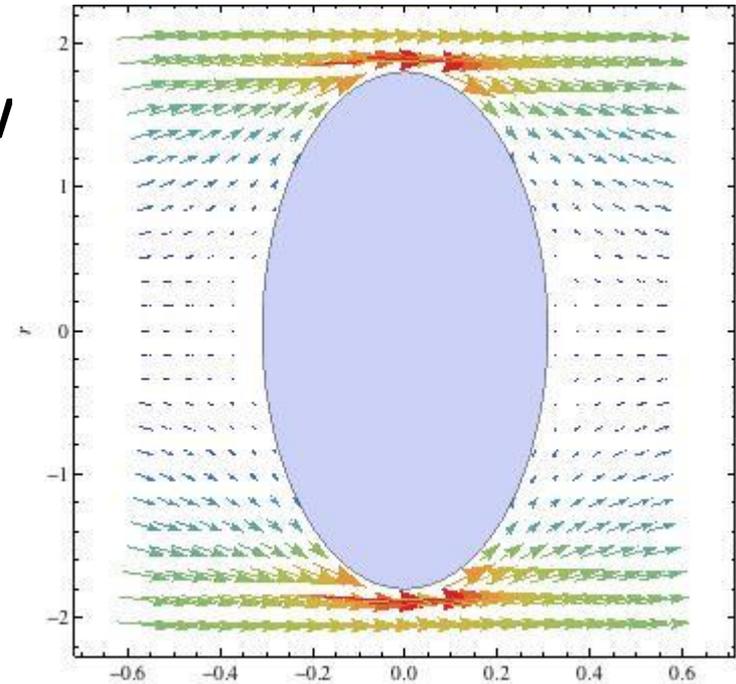
$$U_z = \frac{-1}{r} \frac{\partial \psi}{\partial r}$$

$$U_r = \frac{1}{r} \frac{\partial \psi}{\partial z}$$

$$\psi = \frac{-\frac{1}{2}U_\infty (a^2 - b^2)}{e\sqrt{1-e^2} - \sin^{-1}(e)} \left( \sinh(\xi) - \cosh^2(\xi) \cot^{-1}(\sinh(\xi)) \right) \sin^2(\eta) - \frac{1}{2}U_\infty r(\xi, \eta)^2$$

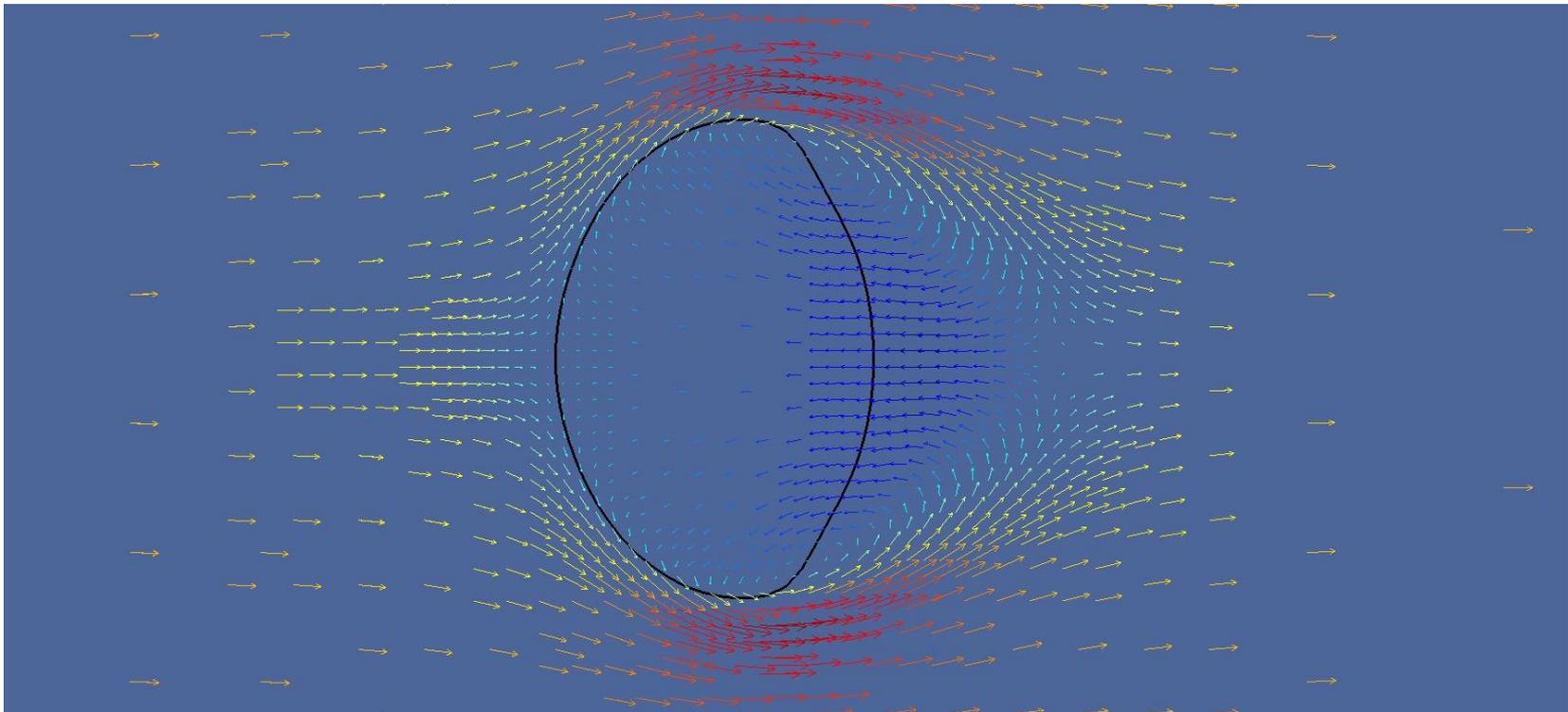
- Conformal transformation

$$z + ir = \sqrt{a^2 - b^2} \sinh(\xi + i\eta)$$



# Not that bad approximation

- Gerris Simulation (Azzara, 2014)



# Kinetic Energy Term

- Can be computed

$$K = \frac{1}{2} \rho_L \iiint_{V(t)} \mathbf{V}^2 d^3x = \frac{1}{2} \rho_L \left( \frac{\dot{y}}{y} \right)^2 \iint_{\text{Ellipse}(yR_0, R_0/y^2)} (r^2 + 2z^2) 2\pi r dr dz$$

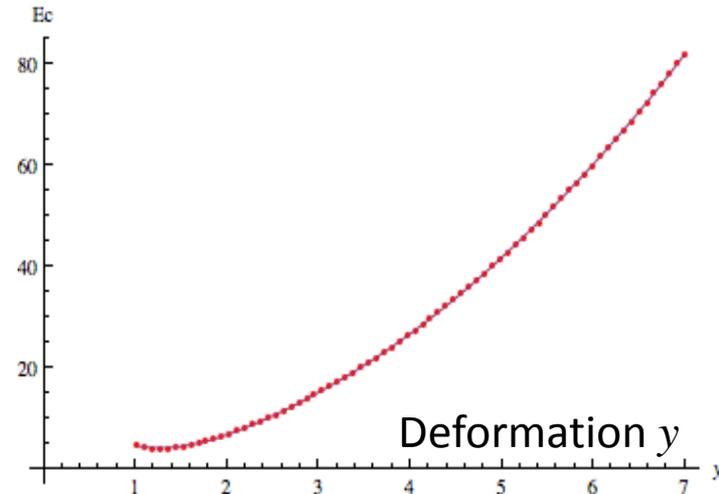
– Thanks to Mathematica!

– And given the shape

$$K = \frac{1}{2} \rho_L K_C(y) \left( \frac{\dot{y}}{y} \right)^2$$

– Where

- $K_c(y) \approx 22.1797 - 36.5808y + 25.9328y^2 - 8.2371y^3 + 1.5115y^4 - 0.1425y^5 + 0.0054y^6$



# Surface Energy Term

- Exact formula (oblate)

$$S = 2\pi a^2 + \pi \frac{b^2}{e} \text{Log} \left( \frac{1+e}{1-e} \right) \quad e = \sqrt{1 - \frac{a^2}{b^2}}$$

- One gets

$$\frac{dE_s}{dt} = \sigma \frac{dE_s}{dy} \frac{dy}{dt} = \sigma K_s(y) \frac{1}{y} \frac{dy}{dt}$$

- Where  $K_s$  can be approximated by

$$K_s(y) \approx -39.682 + 41.523 y - 5.242 y^2 + 3.818 y^3 - 0.404 y^4 + 0.017 y^5$$

# Viscous Dissipation Term

- Cylindrical coordinates

$$D = \mu_L \int_V 2 \left[ \left( \frac{\partial V_r}{\partial r} \right)^2 + \left( \frac{\partial V_\theta}{r \partial \theta} + \frac{V_r}{r} \right)^2 + \left( \frac{\partial V_z}{\partial z} \right)^2 \right] + \left[ \left( r \frac{\partial V_\theta / r}{\partial r} \right) + \frac{\partial V_r}{r \partial \theta} \right]^2 + \left[ \frac{\partial V_z}{r \partial \theta} + \frac{\partial V_\theta}{\partial z} \right]^2 + \left[ \frac{\partial V_r}{\partial z} + \frac{\partial V_z}{\partial r} \right]^2 d^3x$$

- Can be computed exactly

$$D = \mu_L \iiint_{S(y)} 12 \left( \frac{\dot{y}}{y} \right)^2 d^3x = 16\pi R_0^3 \mu_L \left( \frac{\dot{y}}{y} \right)^2$$

– Schmehl et al. (ILASS 2002)

# Air Pressure Work

- Air pressure work is given by

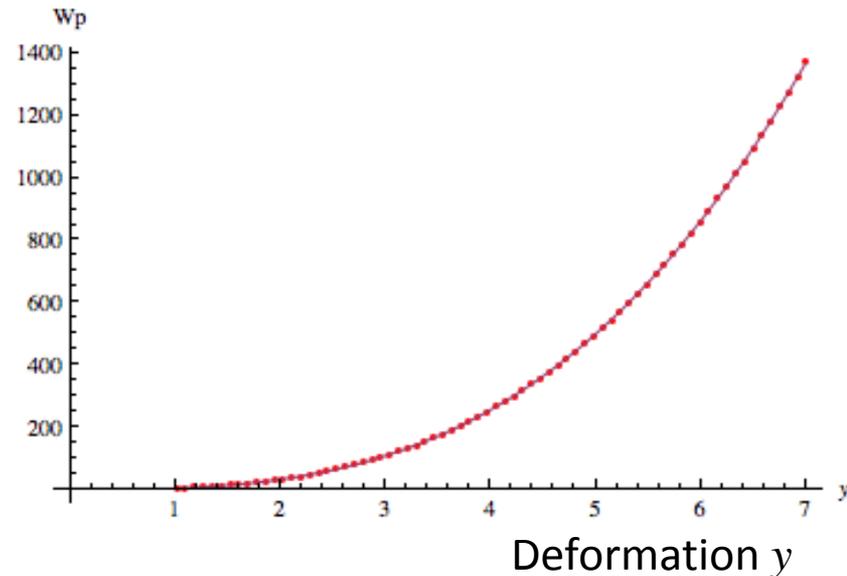
$$W_P = -\oint_{\partial V} P(\mathbf{V} \cdot \mathbf{n}) dS = 2 \int_0^a \frac{1}{2} \mathbf{U}^2 (\mathbf{V} \cdot \mathbf{n}) 2\pi r dr$$

- Which can be given by

$$W_P = \rho_G U_\infty^2 R_0^2 K_P(y) \frac{dy}{dt}$$

- Where

$$K_P(y) \approx -0.599 + 0.535y - 0.178y^2 + 4.026y^3 - 0.00137y^4$$



# Final Equation

- Using non dimensional numbers:

$$K = \frac{\rho_L}{\rho_G} \quad We_G = \frac{\rho_G U_\infty^2 2R_0}{\sigma} \quad Re = \frac{\sqrt{\rho_G \rho_L} U_\infty 2R_0}{\mu_L}$$

$$Oh = \frac{\mu_L}{\sqrt{\sigma_L 2R_0}} \quad \tau = \sqrt{\frac{\rho_G}{\rho_L} \frac{2R_0}{U_\infty}} \quad t^* = \frac{t}{\tau}$$

- One gets:

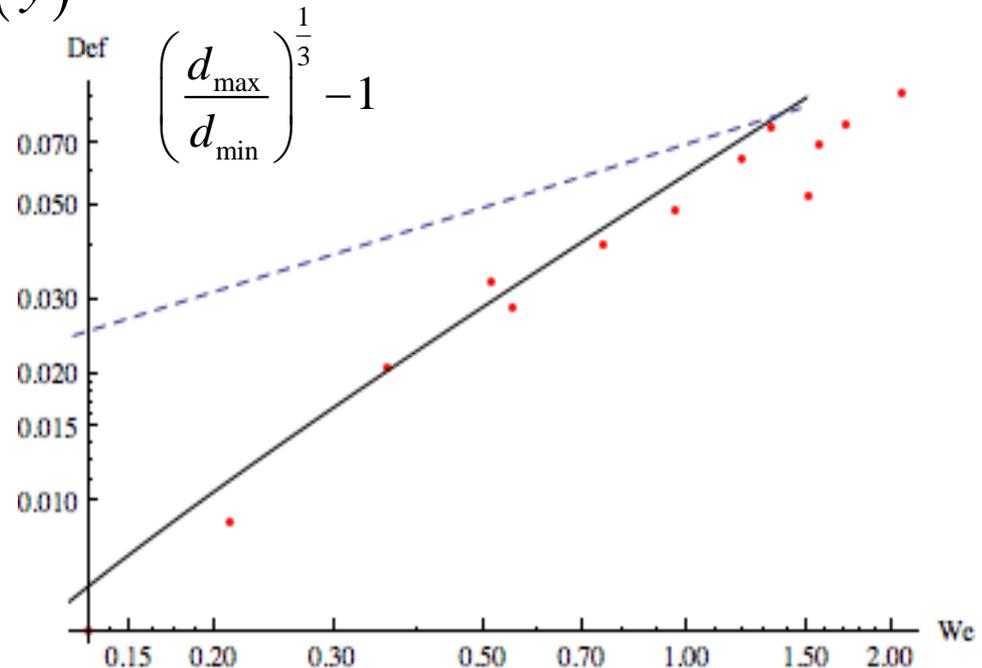
$$\frac{d}{dt^*} \left( \left( \frac{\dot{y}}{y} \right)^2 K_C(y) \right) + \frac{128\pi}{Re} \left( \frac{\dot{y}}{y} \right)^2 + \frac{16}{We_G} K_S(y) \left( \frac{\dot{y}}{y} \right) = 8K_P(y) \left( \frac{\dot{y}}{y} \right)$$

# Steady State

- Equating Air Pressure and Surface Tension

$$We_G = \frac{2K_S(y)}{K_P(y)}$$

- Compare with experimental data (Liquid/liquid)  
*Hsiang & Faeth (1995)*



# Unsteady behavior

- Linearisation  $\varepsilon = y - 1$

$$K_c(1)\ddot{\varepsilon} + \frac{64\pi}{Re}\dot{\varepsilon} + \left(\frac{8}{We}\alpha_2 - 4\beta_2\right)\varepsilon = 0$$

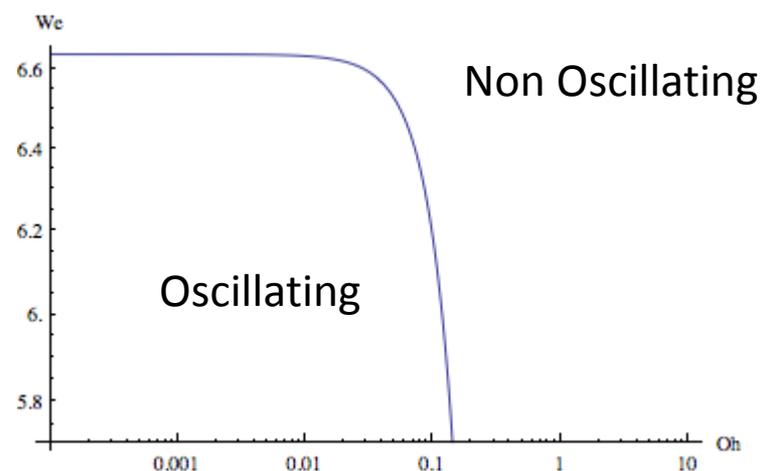
$$We_c = \frac{2\alpha_2}{\beta_2}$$

- Discriminant

$$\Delta = \left(\frac{64\pi}{Re}\right)^2 - 4K_c(1)\left(\frac{8\alpha_2}{We} - 4\beta_2\right)$$

- Oscillating condition

$$Oh^2 < \frac{4K_c(1)}{(64\pi)^2}(8\alpha_2 - 4\beta_2 We)$$



$$Oh_c = \frac{\sqrt{32K_c(1)\alpha_2}}{64\pi}$$

# Decelerating (wind tunnel) drop

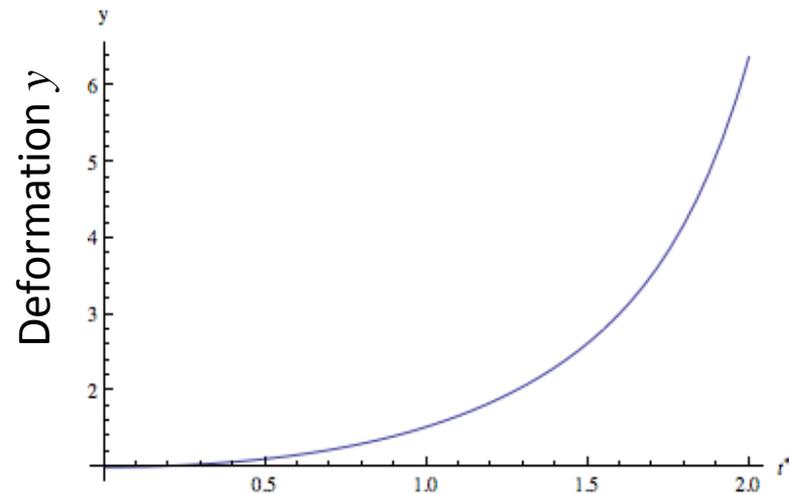
- Non dimensionalisation

–  $U_0$  initial velocity  $U^* = \frac{U}{U_0}$

- Momentum equation

$$\frac{dU^*}{dt^*} = -\frac{3}{2\sqrt{K}} C_d y^{*2} U^{*2}$$

$$C_d(y, Re) = \frac{24}{Re} (1 + 0.1935 Re^{.6305}) \text{Min} \left[ \frac{3y^3 + 4}{7}, 4 \right]$$



$U = 14 \text{ m/s}$   $We = 11.3$ ,  $Oh = 0.006$ ,  $K = 769$

- Deformation equation

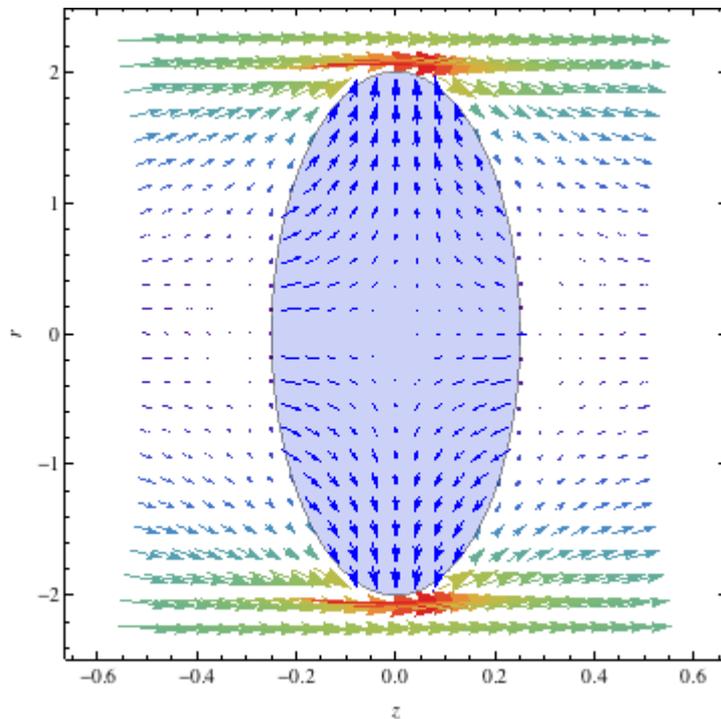
$$2 \frac{d}{dt^*} \left( \left( \frac{\dot{y}}{y} \right)^2 K_C(y) \right) + \frac{128\pi}{Re} \frac{1}{U^*} \left( \frac{\dot{y}}{y} \right)^2 + \frac{16}{We_G} K_S(y) \frac{1}{U^{*2}} \left( \frac{\dot{y}}{y} \right) = \frac{8}{2} K_P(y) \left( \frac{\dot{y}}{y} \right)$$

Vortices inside

Vortices outside

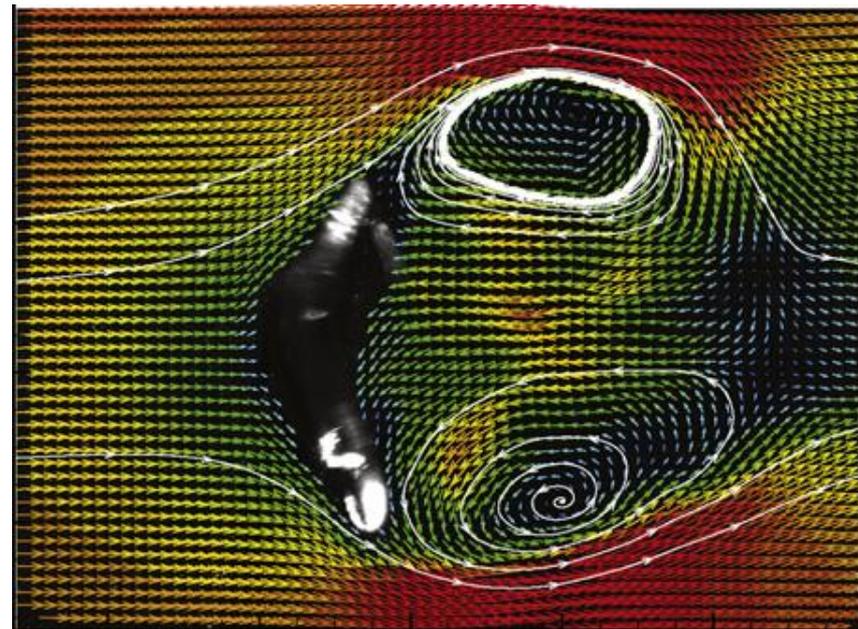
# Why Fitting parameters?

« Model »

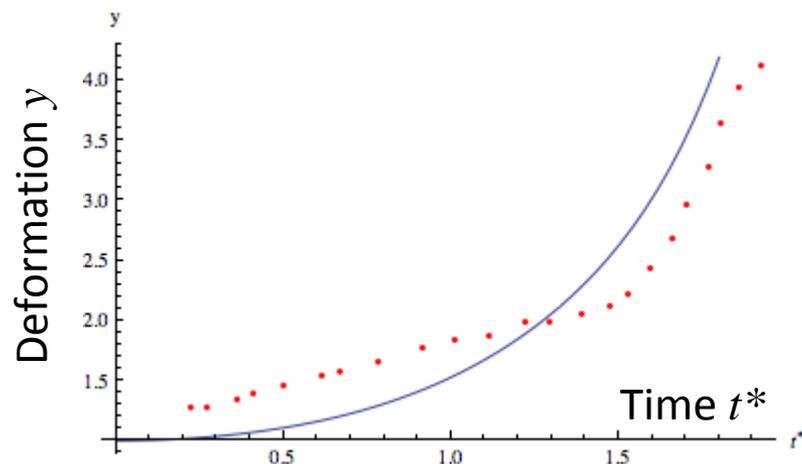


« Reality »

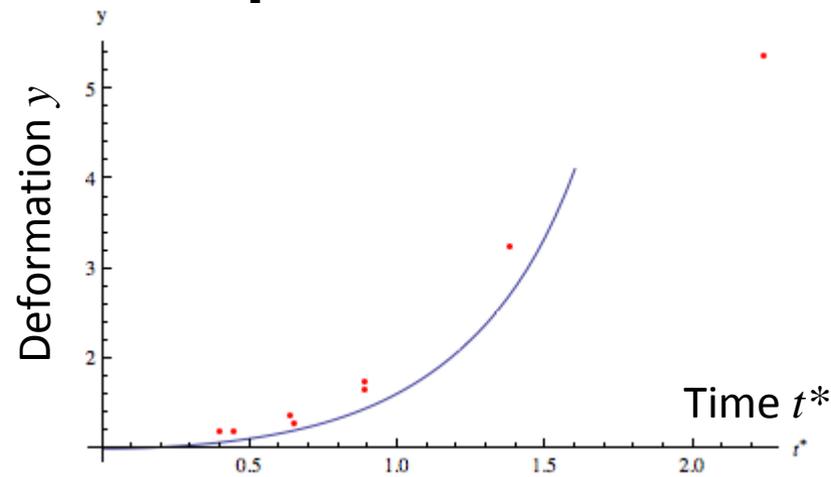
*Flock et al. (2012)*



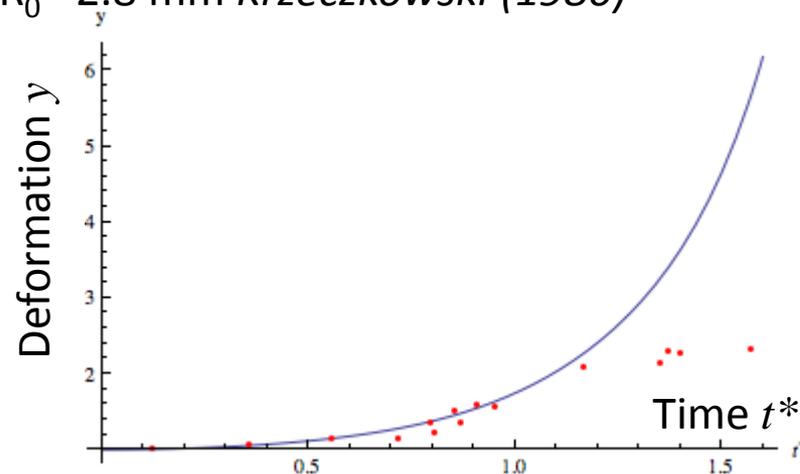
# Comparison with experiments



$U = 14 \text{ m/s}$   $We = 11.3$ ,  $Oh = 0.002$ ,  $K = 769$ .  
 $R_0 = 1.6 \text{ mm}$  *Opfer et al. (2014)*



$U = 13.5 \text{ m/s}$   $We = 18.4$ ,  $Oh = 0.0014$ ,  $K = 770$ .  
 $R_0 = 2.8 \text{ mm}$  *Krzczkowski (1980)*



$U = 32 \text{ m/s}$   $We = 103.5$ ,  $Oh = 0.0014$ ,  $K = 770$ .  
 $R_0 = 2.8 \text{ mm}$  *Krzczkowski (1980)*

# Accelerating (freefall) drop

- Non dimensionalisation

$$Eo = \frac{(\rho_L - \rho_G) g (2R_0)}{\sigma}$$

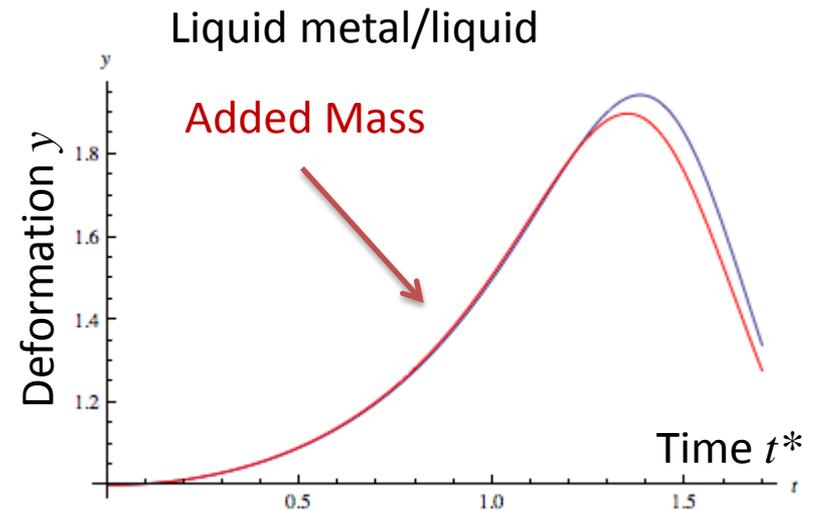
$$U_l = \sqrt{\frac{4(K-1)R_0}{3gC_d}}$$

- Momentum equation

$$\frac{dU^*}{dt^*} = -\frac{3}{2\sqrt{K}} C_d y^{*2} U^{*2} + \frac{K^{3/2}}{K-1} \frac{Eo}{We_G}$$

– Added mass effect

$$\left( 1 + y^3 \frac{1}{K} \frac{e - (\sin^{-1} e) \sqrt{1-e^2}}{\sin^{-1} e - e \sqrt{1-e^2}} \right) \frac{dU^*}{dt^*} = -\frac{3}{2\sqrt{K}} C_d y^{*2} U^{*2} + \frac{K^{3/2}}{K-1} \frac{Eo}{We_G}$$



$U_l = 1.05$  m/s,  $We = 26.88$ ,  $Oh = 0.00014$ ,  
 $K = 8$ ,  $R_0 = 6$  mm

# WHAT HAPPENS WHEN SIZE DOUBLE?

# Rayleigh-Taylor Growth

- Most amplified wavelength is given by

$$\lambda_{RT,\max} = 2\pi \sqrt{\frac{3\gamma}{f\Delta\rho}}$$

- Droplet deceleration is given by

$$f = \frac{3}{8} \frac{\rho_G}{\rho_L} \frac{x^2}{r^3} C_d U^2$$

- Which turns to

$$\frac{\lambda_{RT,\max}}{r} = 2\pi \left( \frac{r}{x} \right) \sqrt{\frac{8\gamma}{C_d \rho_G U^2 r}}$$

- $C_d$  is equal to (Pilch et Erdman, 1987)
  - 1.7 (falling droplet)
  - 3.0 (shock tube)

# Critical Weber Number

- By assuming the following two-waves breakup condition:  $x = \lambda = 2r$ , one gets:

$$\left(\frac{x}{r}\right)^4 = 2^4 = 16 = 64\pi^2 \frac{1}{C_d We}$$

- Which turns to

- Free Fall

- Shock tube

$$We_{\min} = \frac{4\pi^2}{C_d} \approx 23.2$$

$$We_{\min} = \frac{4\pi^2}{C_d} \approx 13$$

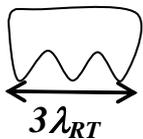
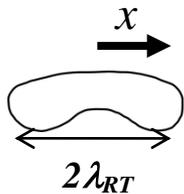
- With three waves

- Umbrella breakup

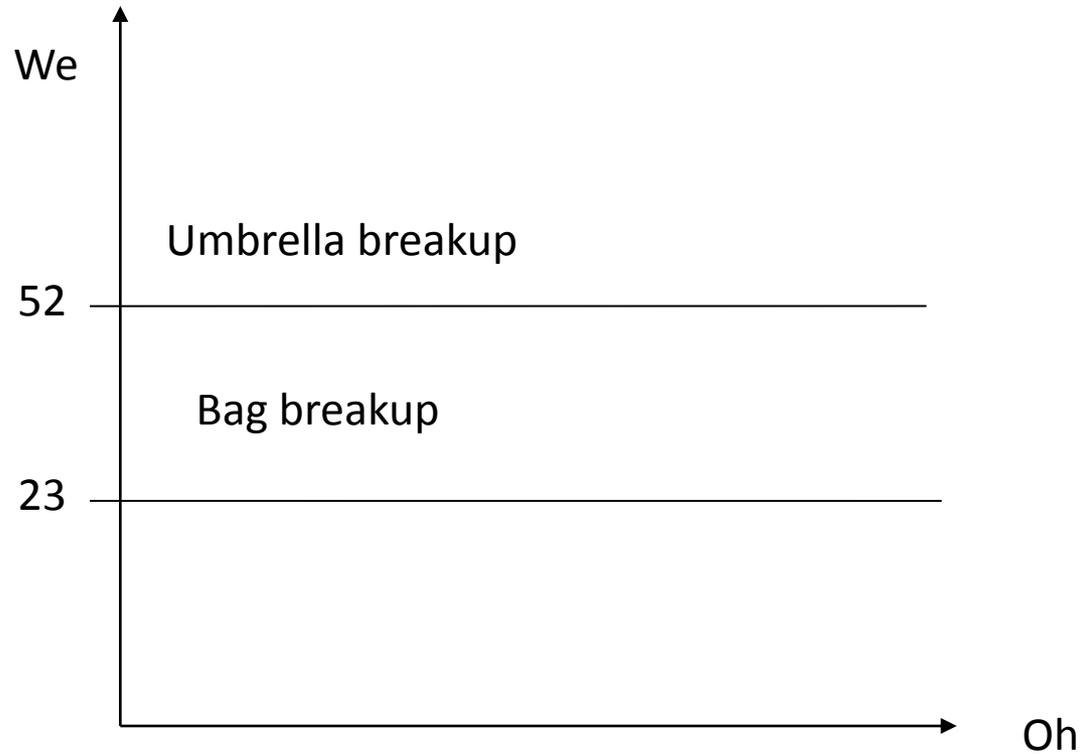
$$2x = 3\lambda_{RT}$$

$$\left(\frac{x}{r}\right)^4 = 12^2 \pi^2 \frac{1}{C_d We}$$

$$We_{\min} = \frac{144\pi^2}{16C_d} = 52 \text{ (chute libre)}$$



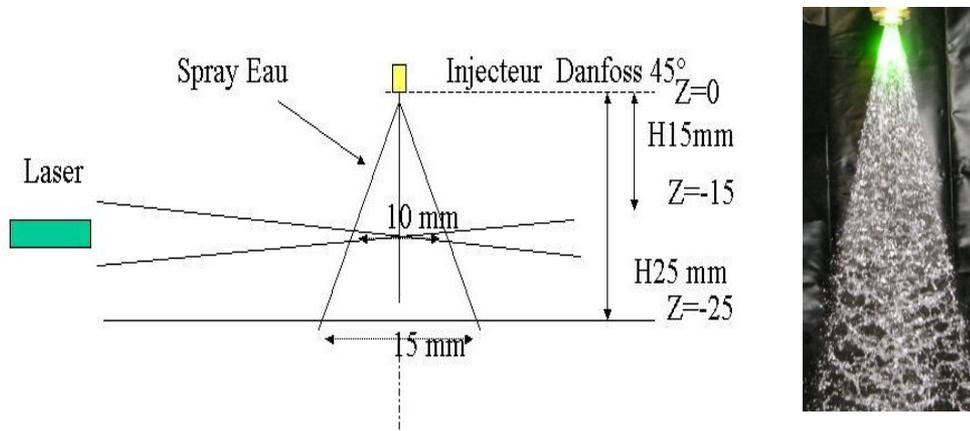
# Theoretical Diagram



# DAUGHTER DROPS PDF

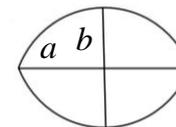
# Bag Breakup

## Dispositif Experimental



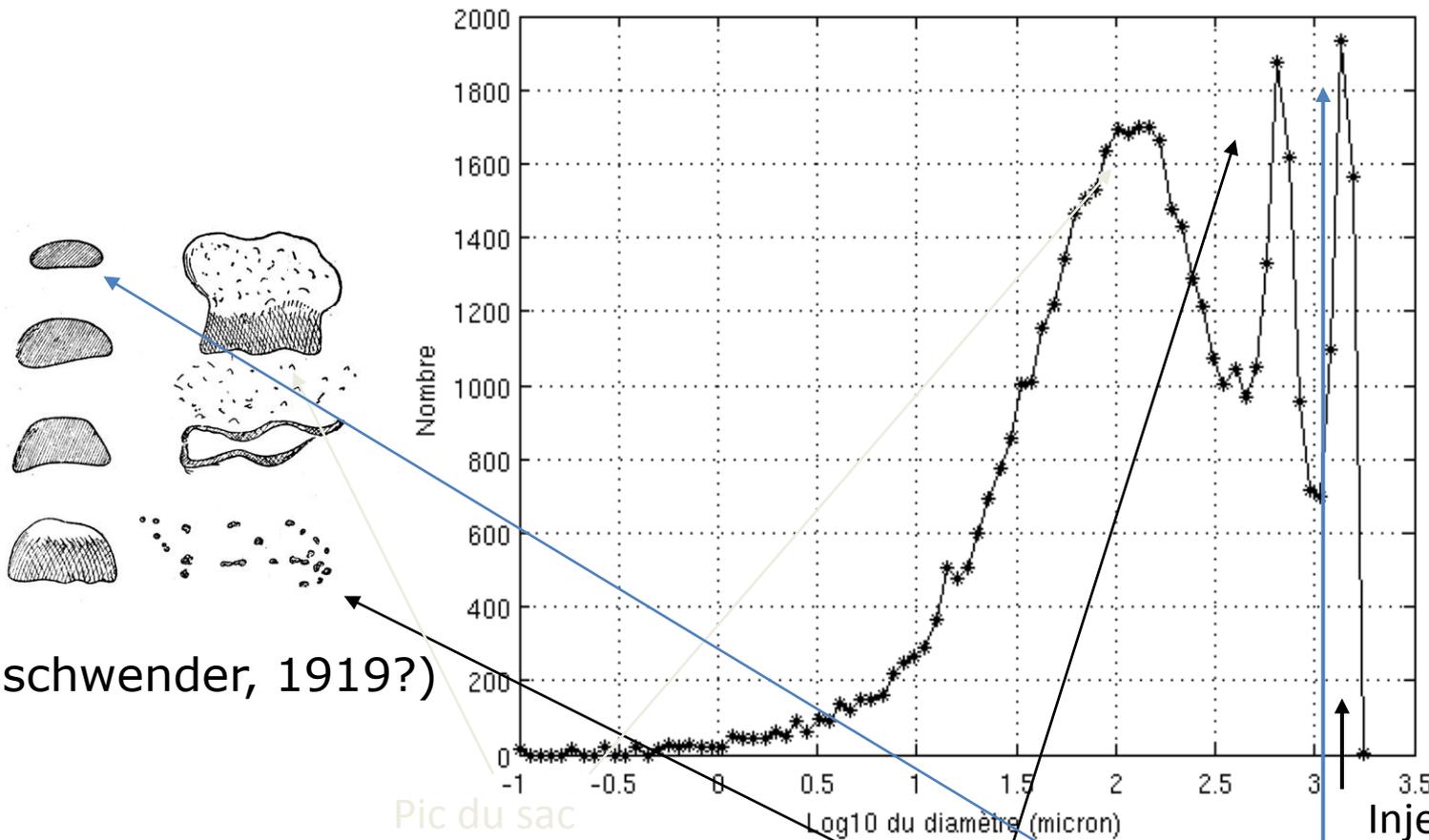
N. Rimbert and G. Castanet *Evidences of turbulent cascading atomization in the bag-breakup regime* Phys. Rev. E (2011)

- **Tuyère Lechler ref. 665-042, 8 bars**
  - Montée verticalement
  - Oeil de chat, "Fan spray", 80 L/minute
- La lumière Laser est guidée optiquement dans une fibre
- PDPA: mesure la taille et la vitesse des gouttes



# PDF à trois pics

Distribution marginale des diamètres



(Hochschwender, 1919?)

Pic du sac

$$\frac{SMD_{bag}}{d_{init}} = \frac{200}{1350} \approx 0.148$$

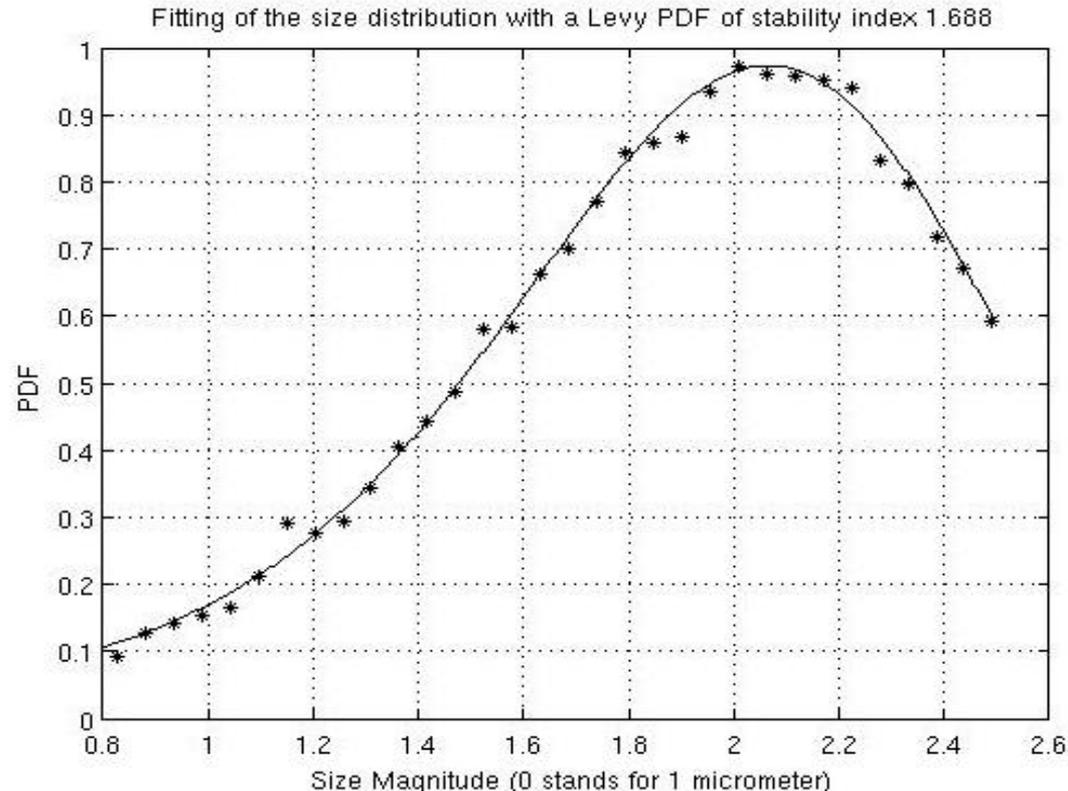
Pic de l'anneau

Pic initial

Injecteur: 3.23

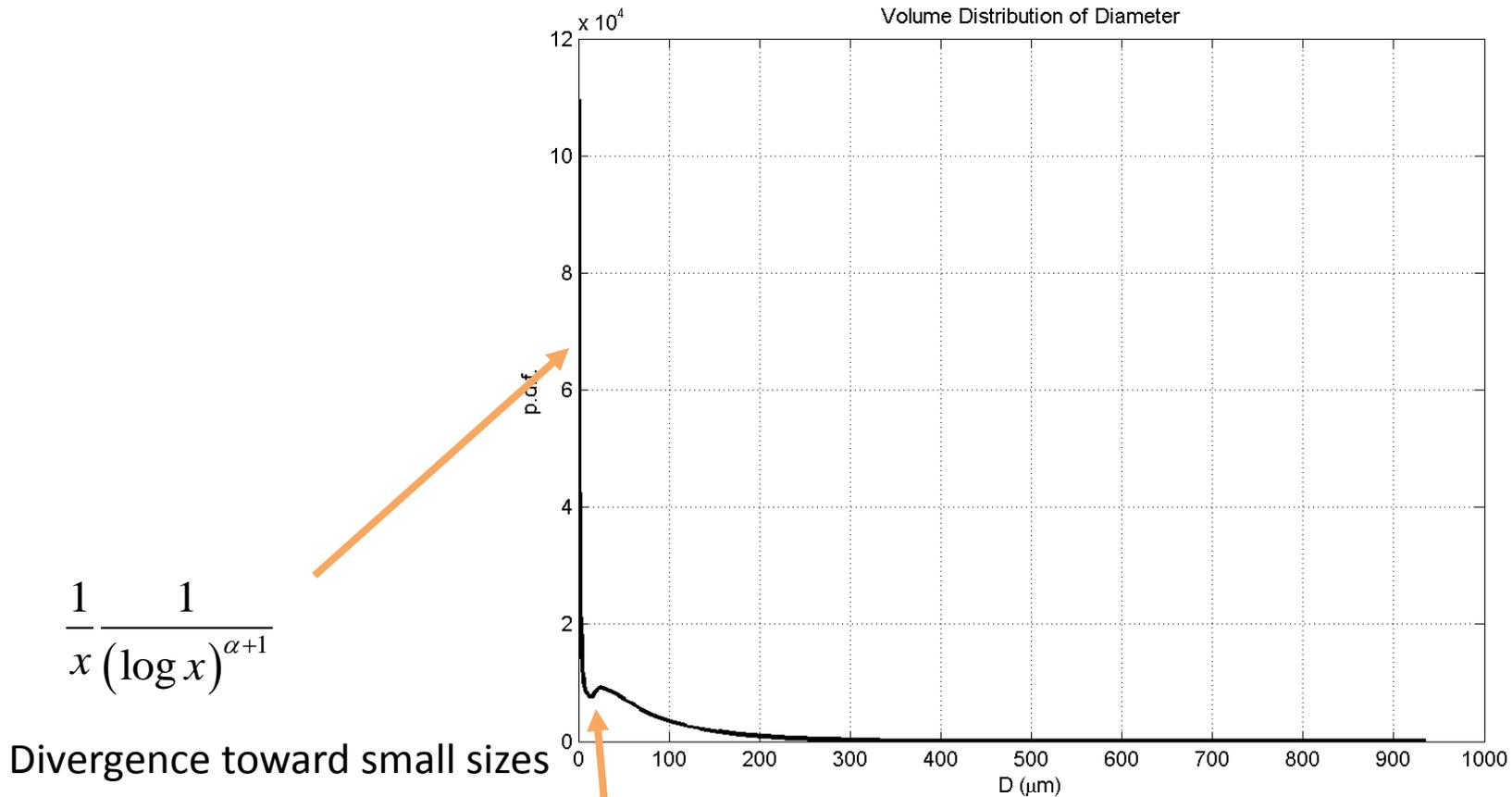
# Log Lévy Stable PDF

- *Novikov and Dommermuth, Phys. Rev. E, 1997*
- *Rimbert and Séro-Guillaume, Phys. Rev. E, 2004*
  - Extension de résultats de Kolmogorov
  - Distribution volumique
  - Données exp. communiquées par Simmons and Hanratty
- Ici, nos propres données
  - 50,000 gouttelettes
  - Distribution numérique
  - $\alpha = 1.69$



$$\sigma_{\ln d} \approx 1.1$$

# Other representation of Log-Lévy PDF



$$\frac{1}{x} \frac{1}{(\log x)^{\alpha+1}}$$

Divergence toward small sizes

Apparently two modes